This presentation premiered at WaterSmart Innovations

watersmartinnovations.com



"Making Water Fracable"



Hydraulic Fracturing Solutions

TERRA Services LLC

Powered by FracSTAR

"Industry leaders in safety and innovation!"

'n



"Making Water Fracable"



TERRA Services LLC

How do you make water "Fracable" if you never look at the water?



The fracturing process uses an average of 230,000 barrels / 9,660,000 gallons of water per well. If only 6 wells are located on a pad. 1,380,000 barrels / 57,960,000 gallons of water per 6 well pad

Well Head Locations

Shale gas fields need many more wells than conventional fields. This illustration shows expansion of a single well to 12 wells from two well pads a half-mile apart within the same square-mile area.

(Images courtesy of frackingboom.com)

FRACKEDWELL





U.S. RIG COUNTS

May 30, 2014

States & Districts	Baker Hughes Rig Count				RigData Rig Count					
	Four Weel	k Average	Last	This	Four Wee	k Average	Last	This	Waiting	
U.S. Land	2013	2014	Week	vveek	2013	2014	Week	Week	to Spud	
Texas RRC District 1	137	118	116	114	136	123	125	123	14	
Texas RRC District 2	87	90	91	90	81	93	91	89	4	
Texas RRC District 3	48	55	53	58	50	64	62	64	3	
Texas RRC District 4	34	35	33	35	31	29	29	25	5	
Texas RRC District 5	13	9	9	9	12	11	12	13	1	
Texas RRC District 6	26	33	34	31	24	33	36	35	1	
Texas RRC District 7B	13	9	10	9	18	18	16	20	7	
Texas RRC District 7C	81	97	97	95	74	102	101	100	7	
Texas RRC District 8	278	326	325	334	265	320	318	316	11	
Texas RRC District 8A	36	38	41	38	34	41	42	37	3	
Texas RRC District 9	21	16	16	16	31	28	30	28	2	
Texas RRC District 10	60	64	62	63	64	67	66	65	0	
Texas Total	834	890	887	892	820	929	928	915	58	

The average well takes 14 days to complete.

890 active drill rigs running for a year will drill 23,203 wells per year

These wells consume would consume 5,336,690,000 Barrels / 224,140,980,000 Gallons of Water each year

July 23-24 2014

NCH Water Reuse Workshop

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No sand, no water, no frac

No frac will take place unless the sand is on hand to complete the stages that are scheduled during a 24hr period.

By the same measure, if there is no water to carry the sand (Proppant) into the formation, there will be NO FRAC.

Water is the most important medium, and part of the Frac. It's the safety, the rinse (Flush) and the carrier of the sand that holds the formation open to let the oil and gas escape.

Water delivery systems to location

Pumped through pipes that can travel for many miles with no treatment of bacteria







How is water currently used?

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- Water for at least one stage, and/or the number of stages to be completed for the first 24hrs, is on hand at location
- Most locations have a set of working tanks to hold a minimum amount of water that is needed to start the fracturing process
- The amount of water is considered a safety feature should a loss of water being delivered to the frac. As a safety an amount of water will be needed to flush the sand from the pumping equipment and the casing to avoid a screen out.

Water Storage

Does the bacteria count go up, down or stay the same?







Test #1 Pit For Fracing		ClO ₂ Residuals							Untreated Water Cultures	
50,000 Barrel Pit		Immediate				Immediate	Source (Coming Into Unit)			
Date	Stage	A1 ClO ₂ Res.	A2 ClO ₂ Res.	Average ClO ₂ Res.	ClO ₂ Res	ClO ₂ Res	Average ClO ₂ Res	SRB (col/ml)	APB (col/ml)	
10/15/2009	Sample #1 @ Pump #1							10,000,000	1,000,000	
10/15/2009	Sample #2 @ Pump #2							1,000,000	1,000,000	
10/15/2009	Time Sample #3	10.22	11.00	10.61	2.33	1.89	2.11	n/a	n/a	
10/15/2009	Time Sample #4	5.30	6.69	6.00	1.12	0.43	0.78	n/a	n/a	
10/15/2009	Time Sample #5	6.47	1.73	4.10	0.77	0.08	0.43	n/a	n/a	
10/15/2009	Time Sample #6	3.31	1.75	2.53	1.12	0.14	0.63	n/a	n/a	
10/15/2009	Time Sample #7	5.30	2.21	3.76	2.88	1.09	1.99	n/a	n/a	
10/15/2009	Time Sample #8	4.20	8.00	6.10	1.62	1.99	1.81	n/a	n/a	
10/15/2009	Time Sample #9	1.38	4.89	3.14	0.01	0.72	0.37	n/a	n/a	
10/15/2009	Time Sample #10	4.92	7.11	6.02	1.44	2.01	1.73	n/a	n/a	
10/15/2009	Time Sample #11	5.88	6.54	6.21	2.44	1.88	2.16	n/a	n/a	
10/15/2009	Time Sample #12	4.10	5.21	4.66	2.04	1.77	1.91	n/a	n/a	
	Averages	5.11	5.51	5.31	1.58	1.20	1.39			

NCH CORPOR Genesis Trailer



•24' Bumper Pull trailer

- •10' Armadillo Trailer
- 2 Armadillo Lines with NO blending capabilities
- •Treat 238 bbls/min
- •456 Points of measurement







Date / Time

Tark #1 (1,02













Test #2 Fra	c #1	CIO ₂ Res	iduals		Treated	l Samples	Untreated W	ater Cultures
120,000 Barre	el Pit	Inlet Manifold to the Working Tanks			at Blender		Source (Coming Into Unit)	
Date	Stage	Amadillo #1	Amadillo #2	Average	SRB (col/ml)	APB (col/ml)	SRB (col/ml)	APB (col/ml)
Filling Tanks	Sample #1 @ Inlet Armadillo #1						100,000	1,000
Filling Tanks	Sample #2 @ Inlet Armadillo #2						10,000	100,000
Stage 1	Time Sample #3	7.40	2.44	4.92	1,000	100	n/a	n/a
Stage 2	Time Sample #4	5.33	6.88	6.11	10,000	1,000	n/a	n/a
Stage 3	Time Sample #5	4.21	3.11	3.66	1,000	1,000	n/a	n/a
Stage 4	Time Sample #6	2.55	1.21	1.88	100	0	n/a	n/a
Stage 5	Time Sample #7	5.44	2.07	3.76	10	100	n/a	n/a
Stage 6	Time Sample #8	3.22	4.01	3.62	0	1,000	n/a	n/a
Stage 7	Time Sample #9	0.88	5.12	3.00	0	0	n/a	n/a
Stage 8	Time Sample #10	2.93	1.65	2.29	10	10	n/a	n/a
Stage 9	Time Sample #11	1.47	0.53	1.00	100	1,000	n/a	n/a
Stage 10	Time Sample #12	3.72	3.01	3.37	10	10	n/a	n/a
Stage 11	Time Sample #12	2.99	1.85	2.42	0	0	n/a	n/a
	Averages	3.65	2.90	3.27	100	1,000	n/a	n/a
Test #2 Fra	c #1	CIO ₂ Residu	uals					
120,000 Barrel Pit		Work	ting Frac Tanks					
Date Stage		Frac Tank #1	Frac Tank #2	Frac Tank #3	Frac Tank #4	Average	Blender	
Stage 1	Time Sample #3	2.46	1.01	0.02	0.85	1.09	0.53	
Stage 2	Time Sample #4	1.12	0.55	0.01	0.59	0.57	0.27	
Stage 3	Time Sample #5	0.89	1.55	3.89	2.01	2.09	1.44	
Stage 4	Time Sample #6	1.05	0.23	0.44	1.67	0.85	0.42	
Stage 5	Time Sample #7	3.61	0.74	0.05	0.23	1.43	1.77	
Stage 6	Time Sample #8	2.88	0.68	1.88	0.89	1.58	1.51	
			0.06	1.23	0.99	1.32	1.41	
Stage 7	Time Sample #9	2.10	0.90			-		
Stage 7 Stage 8	Time Sample #9 Time Sample #10	2.10	0.98	0.22	0.49	0.82	0.23	
Stage 7 Stage 8 Stage 9	Time Sample #9 Time Sample #10 Time Sample #11	2.10 1.01 0.88	0.01	0.22	0.49	0.82	0.23	
Stage 7 Stage 8 Stage 9 Stage 10	Time Sample #9 Time Sample #10 Time Sample #11 Time Sample #12	2.10 1.01 0.88 1.52	0.96 0.01 0.02 0.51	0.22 0.44 0.08	0.49 1.12 1.10	0.82 0.68 0.05	0.23 0.51 1.77	
Stage 7 Stage 8 Stage 9 Stage 10 Stage 11	Time Sample #9 Time Sample #10 Time Sample #11 Time Sample #12 Time Sample #12	2.10 1.01 0.88 1.52 1.01	0.96 0.01 0.02 0.51 0.73	0.22 0.44 0.08 0.41	0.49 1.12 1.10 0.30	0.82 0.68 0.05 1.01	0.23 0.51 1.77 0.89	



NCH CORPOPIIOt Frac Research 12-22-09

Source water was high in bacteria

- 9 Stage Frac Test results of Prefrac Bacteria Counts
- SRB's @ 109

 (1,000,000,000 cfu/ml)
 (9 bottles turned)
- APB's @ 104

 (10,000 cfu/ml)
 (4 bottles turned)



Stage #1 thru Stage #9 CIO2 Residual Summary



Net CIO2 Residual During 222.75 Hrs = 1.05ppm Net CIO2 Residual During Stages Only = 1.46ppm After Stage #3 Best and Worst Frac Tanks

Test results of Bacteria Counts SRB's @ <<u>100 (less than 1 cfu/ml) !!!!</u> APB's @ <<u>100 (less than 1 cfu/ml) !!!!</u> <u>IN ALL TANKS!!!</u>

After Stage #6 All Frac Tanks #1 to #4



Test results of Bacteria Counts SRB's @ <<u>100 (less than 1 cfu/ml) !!!!</u> APB's @ <<u>100 (less than 1 cfu/ml) !!!!</u> IN ALL TANKS!!!

Produced Samples 100 Barrels 1-1-10 and 1025 Barrels1-2-10

Test results of Post TERRAfrac Bacteria Counts SRBS @ $<10^{\circ}$ (less than 1 cfu/ml) !!!! APBs @ $<10^{\circ}$ (less than 1 cfu/ml) !!!!

In Produced Water After 100 Barrels & 1025 Barrels !!! 1025 Barrels Sample had a CIO2 Residual of 0.23ppm!! and Chlorides of >18,000ppm



Test #2 Eres	- #2		iduale		T	l Comulta	Underset a date	have Caller
Test #3 Frac #2		CIO ₂ Kes	luuais		Ireated	Samples	Untreated Water Cultures	
90,000 Barrel Frac		Inlet Manifold to the Working Tanks			at Blender		Source (Coming Into Unit)	
Date	Stage	Amadillo #1	Amadillo #2	Average	SRB (col/ml)	APB (col/ml)	SRB (col/ml)	APB (col/ml)
Filling Tanks	Sample #1 @ Inlet Armadillo #1						1,000,000,000	10,000
Stage 1	Time Sample #2	4.22	3.88	4.05	0	0	n/a	n/a
Stage 2	Time Sample #3	5.00	5.50	5.25	0	0	n/a	n/a
Stage 3	Time Sample #4	3.88	4.23	4.06	0	0	n/a	n/a
Stage 4	Time Sample #5	4.11	4.89	4.50	0	0	n/a	n/a
Stage 5	Time Sample #6	5.17	4.86	5.02	0	0	n/a	n/a
Stage 6	Time Sample #7	4.38	3.77	4.08	0	0	n/a	n/a
Stage 7	Time Sample #8	3.65	5.16	4.41	0	0	n/a	n/a
Stage 8	Time Sample #9	4.67	4.44	4.56	0	0	n/a	n/a
Stage 9	Time Sample #10	4.25	4.97	4.61	0	0	n/a	n/a
	Averages	4.37	4.63	4.50	0	0	n/a	n/a
Test #3 Frac	: #2	ClO ₂ Residu	uals					
90,000 Barrel Frac		Working F	rac Tanks					
Date Stage		Frac Tank #1	Frac Tank #2	Frac Tank #3	Frac Tank #4	Average	Blender	
Stage 1	Time Sample #2	3.88	4.00	3.22	2.88	3.50	1.80	
Stage 2	Time Sample #3	4.12	4.44	3.75	3.11	3.86	1.44	
Stage 3	Time Sample #4	3.12	3.51	3.72	3.00	3.34	1.12	
Stage 4	Time Sample #5	3.55	3.44	3.78	3.99	3.69	1.23	
Stage 5	Time Sample #6	4.22	4.89	3.93	3.90	1.43	1.56	
Stage 6	Time Sample #7	3.52	3.10	3.77	3.65	3.51	1.51	
	Time Sample #9	5.01	5.00	1.23	0.99	3.06	1.41	
Stage 7	Time sample #8	5.01						
Stage 7 Stage 8	Time Sample #8	4.02	3.57	3.12	3.96	0.82	1.62	
Stage 7 Stage 8 Stage 9	Time Sample #8 Time Sample #9 Time Sample #10	4.02	3.57 3.38	3.12 3.91	3.96 2.88	0.82 0.68	1.62 1.45	

NAlpha 1 & TION





•42' Gooseneck Trailer

Alpha 2 Trailers

- •Two 10" Armadillo lines and a 6" produced water line
- •6" Produced line blends up to 30/bpm into each Armadillo line
- •Able to treat 240 bpm
- •712 Points of measurement
- Measures armadillo lines and frac tank
 ClO2 residual, conductivity, pH, and pressure
- •Web based
- PID/PLC Control
- •Water treatment test lab
- •Supplies its own power through a generator
- •Eye wash / safety shower



- Average to blender will approach, but not exceed 5PPM because set 5PPM as max per this test and reasearch.



-Able to maintain residual available to blender at steadier rate





NCH CORPORATION Stage 2A Review – Software Calibration



NCH CORPORATION Conductivity Data



Stage 2B Conductivity at Frac Tanks



Stage 3A Conductivity Frac Tanks



Stage 3B Conductivity Frac Tanks





Stage 3A pH at Frac Tanks



Terra Frac #1.01-021403 - System pH 06/22/10 10:00 - 06/22/10 11:15 14.0 - SYS1 pH Avg: 6.2 Min: 4.8 Max: 6.9 Hq: MOU 11.2 8.4 5.6 2.8 0.0 06/22/10 10:00 06/22/10 10:37 06/22/10 11:15 Date / Time

Stage 2B pH at Frac Tanks



Stage 3B pH at Frac Tanks



FracSTAR is a custom built proprietary hardware and software package to integrate points of measurement used in the TerraFrac process. It allows for the blending and treatment of water used in the fracturing process. FracSTAR models the water 100 times per second and can predict the bio-demand to control the blends of reuse and recycled waters.



The TERRA trailer is a mobile water treatment plant/process that treats water using Chlorine Dioxide (ClO_{2}) to remove all bacteria from water used in hydraulic fracturing. The FracSTAR technology operates in real-time, with 1,489 points of continuous measurements with a proprietary custom built operating system at flow rates of over 345 barrels per minute (BPM). The FracSTAR system is the safest, most advanced form of water treatment using Chlorine Dioxide (ClO₂) that has ever been developed for hydraulic fracturing.



The FracSTAR mobile frac water treatment process was built around water use during the hydraulic fracturing process. It can process large volumes of water, at high velocities, and deliver a 99.9999999% bacteria kill



The TERRA unit was built to follow the same on-pad model as horsepower; first equipment on location and last off. Every drop of water used in the fracturing of an oil & gas well will flow through the TERRA trailer process.

The TERRA trailer has three separate water inlets:

- <u>Armadillo line #1</u> is a 10" fresh water inlet 142.00 BPM / 6,000 GPM
- <u>Armadillo line #2</u> is a 10" fresh water inlet 142.00 BPM / 6,000 GPM
- <u>Produce Water</u> is a 6" waste water inlet 59.00 BPM / 2,500 GPM

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The TERRA trailer replaces the traditional water transfer distribution manifold. This is to insure that all water passes through the FracSTAR process so that every drop of water is not only measured, but treated. The FracSTAR process can treat between 4 and 8 working tanks.



Recycle / Reuse Blending Into Armadillo Line #1 & #2





The TERRA trailer has nine separate outlets.

<u>Armadillo Line #1</u> has four 6" outlets <u>Armadillo Line #2</u> has four 6" outlets <u>Produce Water Line</u> has one 6" outlet



All water being treated is plumbed to the sink in the Lab/Control Room to gather samples and run tests without the operator leaving the trailer





Safe environment that is controlled to insure safety and allow for maintenance and calibrations of sensors and meters


Frac Water Treatment 3D Control





Total Frac Water Inlet Stage 1

➡ BPM ━━ Lowest BPM ━━ Highest BPM ━━ Average BPM (60 Seconds)









8/20/2013 1:53:00 PM to 8/20/2013 3:33:00 PM

Field Evaluation Case Study

The FracStar control process will send information to two locations :

1) The frac van

 2) Water Transfer and the working frac tanks
This information will be displayed on iPads ,









NCH CORPORATION Monitoring Equipment



NCH CORPORATION Monitoring Equipment







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Before Treatment

Pre-treatment demand averaged 10¹² APB's and SRB's

During CIO₂ Treatment (Its Green) During CIO₂ Treatment Iron Sulfide SRB Sludge



Post Treatment

After CIO₂ treatment Iron Sulfide oxidized into SO4 and Fe3 SRB bacteria dead and floating on top of water like dead fish



Post Treatment





10⁰ APB's and 10⁰ SRB's





Reusable water for the next frac





FracSTAR Development Plan

- Total water management
- Zero water foot print
- Treatment concepts
- Stationary plants
- Blending and reuse on-the-fly development





Barium Sulfate Scale (BaSO4) with Iron (Fe3)





2" Diameter ¼" Buildup

NCH CORPORATION Solids down in the formation



Sand Down in the formation

7

SPE 165085

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Fig. 6—Representative images of 20/40-mesh ceramic proppant 30 min after introducing (a) Permian produced water, and (b) ECtreated Permian produced water at the flow rate of 100 mL/min.



Fig. 7—Representative images of 20/40-mesh ceramic proppant 30 min after introducing (a) Marcellus produced water, and (b) ECtreated Marcellus produced water at the flow rate of 100 mL/min.

Reuse & Recycle Processes

- Treatment and isolation (non-blending processes)
- Centralized facility

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- Mobile reuse & recycle
- The need to balance the water to make it fracable and remove:
 - TSS (Total Suspended Solids)
 - Soluble divalent cation's and transition metals that will become insoluble
 - Oil and other TPH's (Total Petroleum Hydrocarbons)
 - Bacteria (MOST IMPORTANT)
 - Do not put bacteria down hole and seed the formation

Six bottles turned = 10⁶(1,000,000) CFU (Colony Forming Unit) of APB (Acid Producing Bacteria)



Three bottles turned = $10^{3}(1,000)$ CFU (Colony Forming Unit) Of SRB (Sulfate Reducing Bacteria)

NCH Water Reuse Workshop



Hydraulic Fracturing Solutions Powered by FracSTAR





"Industry leaders in safety and innovation!"

TERRA Services Unit

Continuous of operation for operators who want to recycle untreated flowback and produced water on-the-fly and let the pump service company's (Horsepower) control the blends/mixing.

The treatment program consists of oxidation to insure no bacteria, and the monitoring of pH residual in the post treated water. 323+ wells 23% Water reused & recycled 17,086,700 barrels / 717,641,400 gallons of water reclaimed

with an average disposal rate of **\$4.20** for disposal. The producer saved **\$71,764,140** in disposal cost.

This FracStar Dashboard takes into account the different waters and their make-up that would be blended with fresh waters to not affect the sand (proppant) chemistry. This helps to insure of no pressure increases and/or flow rate decreases going down hole during the fracturing process.





Specs for chemistry that will carry the sand (proppant). Variances that would affect the frac performance are identified.

FracStar was developed to micromanage the properties of the water to be used on the frac, and in the treatment of water that would be recycled and reused on the next frac. The Cation and Anions relationship must be considered in order to insure that the water is "fracable"

Reus	e & Recycle (Eagleford)	Treated W	ater Comparison							
	Location	Date	Indice	Untreated	Treated	EOG Specs (<)	Spec Variance	Dilution Value	Variance	
	Orr Ranch 1H	11/20/2013	рН	5.9	8.1	5.0 - 8.0	(0.100)		1	
			Hardness (mg/l)	37,236	44,462	2,000	42,462.000	2,470.11	(470.11)	
	Barrels Per Stage	9,000.00	Specific Gravity (g/ccm)	1.094	1.084	1.038	0.046	0.06	0.00	
			TDS (mg/l)	132,830	115,172	120,000	(4,828.000)	6,398.44	0.00	
	Stages Per Day	5.00	H2S (mg/l)	1	0		0.000	0.00	0.00	
			CO2 (mg/l)	127.96	7.51		7.510	0.42	0.00	
	Barrels of Treated Water		Resistivity	0.072	0.073		0.073	0.00 0.00		
	Total Volume Per Day	2,500.00	Barium (mg/l)	0.01	0.01	10	(9.990)	0.00	0.00	
			Calcium (mg/l)	11,360	11,680	1,000	10,680.000	2,470.11 (470.11) 0.06 0.00 6,398.44 0.00 0.00 0.00 0.42 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.02 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00 1,409.00 0.00 0.00 0.00 4,044.44 0.00 4,02 0.00 47.33 0.00 0.00 0.00 4,134.50 0.00		
			Iron (mg/l)	3.86	0.32	10	(9.680)	0.02	0.00	
ter	Total Volume of Resue		Magnesium (mg/l)	2,147	3,709	1,200	2,509.000	206.06	206.06 0.00	
	Available Per Stage	45,000.00	Manganese (mg/l)	0.02	0.01	10	(9.990)	0.00	0.00 0.00	
ac,			Potassium (mg/l)	0	0	1,000	(1,000.000)	0.00	0.00	
of	Cycles of Dilution	18.00	Sodium (mg/l)	36,359	25,362	36,000	(10,638.000)	1,409.00	0.00	
			Strontium (mg/l)	0	0	10	(10.000)	0.00	0.00	
	me of Blended Barrels Per Stage	500.00	Total Cations (mg/l)	49,870	40,751		40,751.000	2,263.94	0.00	
lon			Chloride (mg/l)	82,400	72,800	70,000	2,800.000	4,044.44	0.00	
	Dilution Factor	0.056	Carbonate	0	0		0.000	0.00 0.00		
			Bicarbonate	232	769	1,000	(231.000)	42.72	0.00	
			Sulfate	328	852	500	352.000	47.33	0.00	
			Boron	0	0	5	(5.000)	0.00	0.00	
•			Total Anions (mg/l)	82,960	74,421		74,421.000	4,134.50	0.00	
to		Calcite (% Saturation)		0.756	145.91					
ιΟ	Calcite (lbs/		Calcite (lbs/1000 bbls)	-0.00269	1.68					
r is			Gypsum (%Saturation)	0.277	0.676					
			Gypsum (lbs/1000 bbls)	-116.85	-52.14					
			Barite (% Saturation)	0.00527	0.0136					
			Barite (lbs/1000 bbls)	-1.1	-0.429					
			Iron Hydroxide (% Saturation)	0.001	0.001					
			Iron Hydroxide (lbs/1000 bbls)	0.001	0.001					

NCH Water Reuse Workshop

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Reuse & Recycle (Eagleford) - Treated Water Comparison									
Location	Date	Indice	Untreated	Treated	EOG Specs (<)	Spec Variance	Dilution Value	Variance	
Orr Ranch 2H	11/20/2013	pН	5.7	8.3	5.0 - 8.0	(0.300)			
		Hardness (mg/l)	62,434	53,641	2,000	51,641.000	2,980.06	(980.06))
Barrels Per Stage	9,000.00	Specific Gravity (g/ccm)	1.182	1.158	1.038	0.120	0.06	0.00	
		TDS (mg/l)	256,481	223,210	120,000	103,210.000	12,400.56	0.00	Ν
Stages Per Day	5.00	H2S (mg/l)	1	0		0.000	0.00	0.00	
		CO2 (mg/l)	157.44	7.84		7.840	0.44	0.00	
Barrels of Treated Water		Resistivity	0.052	0.053		0.053	0.00	0.00	
Total Volume Per Day	2,500.00	Barium (mg/l)	0.1	0.1	10	(9.900)	0.01	0.00	
		Calcium (mg/l)	21,600	17,440	1,000	16,440.000	968.89	0.00	
		Iron (mg/l)	0.49	0.91	10	(9.090)	0.05	0.00	
Total Volume of Resue		Magnesium (mg/l)	2,050	2,440	1,200	1,240.000	135.56	0.00	
Available Per Stage	45,000.00	Manganese (mg/l)	0.01	0.01	10	(9.990)	0.00	0.00	
		Potassium (mg/l)	0	0	1,000	(1,000.000)	0.00	0.00	
Cycles of Dilution	18.00	Sodium (mg/l)	73,091	64,002	36,000	28,002.000	3,555.67	0.00	
		Strontium (mg/l)	0	0	10	(10.000)	0.00	0.00	
Volume of Blended Barrels Per Stage	500.00	Total Cations (mg/l)	96,741	83,883		83,883.000	4,660.17	0.00	
		Chloride (mg/l)	159,200	137,200	70,000	67,200.000	7,622.22	0.00	
Dilution Factor	0.056	Carbonate	0	0		0.000	0.00	0.00	
		Bicarbonate	293	1,513	1,000	513.000	84.06	0.00	
		Sulfate	247	614	500	114.000	34.11	0.00	
		Boron	0	0	5	(5.000)	0.00	0.00	
		Total Anions (mg/l)	159,740	139,327		139,327.000	7,740.39	0.00	
		Calcite (% Saturation)	0.81	444.48					

FracStar shows the limiting factor being hardness by 980.06 PPM. The water from this field would have to be used at a lower ratio to avoid the "fracablity" of the fluid.

The expense of removing the hardness by chemical and/or mechanical means would have to be deployed.

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Resuse & Recycle (Eagleford) - Treated Water Comparison

FracStar shows that the fluid could be used at greater ratios and not affect the "fracablity" of the fluid.

The spec variance models the water at 100% reuse and identifies the properties that must be diluted and/or treated to be remove.

Location	Date	Indice	Untreated	Treated	EOG Specs (<)	Spec Variance	Dilution Value	Variance	
Orr Ranch 9H	11/20/2013	рН	6.9	8.7	5.0 - 8.0	(0.700)			
		Hardness (mg/l)	34,836	32,437	2,000	30,437.000	1,802.06	0.00	
Barrels Per Stage	9,000.00	Specific Gravity (g/ccm)	1.092	1.080	1.038	0.042	0.06	0.00	
		TDS (mg/l)	129,585	113,724	120,000	(6,276.000)	6,318.00	0.00	
Stages Per Day	5.00	H2S (mg/l)	1	0		0.000	0.00	0.00	
		CO2 (mg/l)	14.67	2.33		2.330	0.13	0.00	
Barrels of Treated Water		Resistivity	0.079	0.081		0.081	0.00	0.00	
Total Volume Per Day	2,500.00	Barium (mg/l)	0.1	0.01	10	(9.990)	0.00	0.00	
		Calcium (mg/l)	10,400	9,280	1,000	8,280.000	515.56	0.00	
		Iron (mg/l)	2.69	0.5	10	(9.500)	0.03	0.00	
Total Volume of Resue		Magnesium (mg/l)	2,147	2,245	1,200	1,045.000	124.72	0.00	
Available Per Stage	45,000.00	Manganese (mg/l)	0.01	0.01	10	(9.990)	0.00	0.00	
		Potassium (mg/l)	0	0	1,000	(1,000.000)	0.00	0.00	
Cycles of Dilution	18.00	Sodium (mg/l)	36,123	30,824	36,000	(5,176.000)	1,712.44	0.00	
		Strontium (mg/l)	0	0	10	(10.000)	0.00	0.00	
Volume of Blended Barrels Per Stage	500.00	Total Cations (mg/l)	48,673	42,349		42,349.000	2,352.72	0.00	
		Chloride (mg/l)	80,400	69,600	70,000	(400.000)	3,866.67	0.00	
Dilution Factor	0.056	Carbonate	0	0		0.000	0.00	0.00	
		Bicarbonate	110	988	1,000	(12.000)	54.89	0.00	
		Sulfate	402	787	500	287.000	43.72	0.00	
		Boron	0	0	5	(5.000)	0.00	0.00	
		Total Anions (mg/l)	80,912	71,375		71,375.000	3,965.28	0.00	
			2.39	339.87					
	Calcite (lbs/1000 bbls) 0.01		0.017	5.07					
	Gypsum (%Saturation)		0.325	0.607					
	Gypsum (lbs/1000 bbls		-119.11	-79.89					
		Barite (% Saturation)	0.0693	0.0165					
		Barite (lbs/1000 bbls)	-0.788	-0.353					
		Iron Hydroxide (% Saturation)	0.001	0.001					
		Iron Hydroxide (lbs/1000 bbls)	0.001	0.001					

Re	euse & Recycle (Eaglef	ford) - Treate	d Water Comparison						
	Location	Date	Indice	Untreated	Treated	EOG Specs (<)	Spec Variance	Diution Value	Variance
	Novak 1H	11/20/2013	pН	6.3	8.2	5.0 - 8.0	(0.200)	/	
			Hardness (mg/l)	5,907	4,304	2,000	2,304.000	239.11	0.00
		9,000.00	Specific Gravity (g/ccm)	1.020	1.020	1.038	(0.018)	0.06	0.00
			TDS (mg/l)	28,959	29,770	120,000	(90,230.000)	1,653.89	0.00
FracStar looks at	the blend,	5.00	H2S (mg/l)	0.5	0		0.000	0.00	0.00
and/or a compos	ite of water		CO2 (mg/l)	173.93	2.58		2.580	0.14	0.00
			Resistivity	0.238	0.229		0.229	0.00	0.00
that was blended	i prior to	2,500.00	Barium (mg/l)	0.01	0.01	10	(9.990)	0.00	0.00
treatment. These	e results		Calcium (mg/l)	1,640	1,360	1,000	360.000	75.56	0.00
show what a 100			Iron (mg/l)	2.84	0.13	10	(9.870)	0.01	0.00
	/016036	45 000 00	Magnesium (mg/l)	439	220	1,200	(980.000)	12.22	0.00
and recycle wate	r would	45,000.00	Manganese (mg/l)	0.01	0.01	1000	(9.995)	0.00	0.00
look like, and the	dilution	18.00	Sodium (mg/l)	8 707	9.652	36.000	(1,000,000)	536.78	0.00
factor when blond	dod with	18.00	Strontium (mg/l)	0	0	10	(10.000)	0.00	0.00
Tactor when blend		ge 500.00	Total Cations (mg/l)	10.789	11.242		11.242.000	624.56	0.00
other fresh water	S.		Chloride (mg/l)	17,300	17,600	70,000	(52,400.000)	977.78	0.00
		0.056	Carbonate	0	0		0.000	0.00	0.00
This way knowing	g what the		Bicarbonate	390	256	1,000	(744.000)	14.22	0.00
water will be afte	r treatment		Sulfate	480	672	500	172.000	37.33	0.00
			Boron	0	0	5	(5.000)	0.00	0.00
neips control the	quality of		Total Anions (mg/l)	18,170	18,528		18,528.000	1,029.33	0.00
the finished prod	uct thereby		Calcite (% Saturation)	0.89	21.93			\	
insuring the perfo	rmance		Calcite (lbs/1000 bbls)	-0.00804	1.84				
			Gypsum (%Saturation)	0.214	0.271				
and the "fracablit	y" of the		Gypsum (lbs/1000 bbls)	-452.08	-463.39				
treated water.			Barite (% Saturation)	0.06	0.0919				
			Barite (lbs/1000 bbls)	-0.0928	-0.0585				
			Iron Hydroxide (% Saturation)	2.76	0.001				
			Iron Hydroxide (Ibs/1000 bbls)	0.001	0.001	1			i i

FracStar shows that this fluid could be used at greater ratios and not affect the "fracablity" of the fluid.

The dilution value models the water at the planned percent of planned reuse, and identifies the properties that must be diluted and/or treated to remove. It also identifies if this water can be used in high concentrations without affecting the performance and the "fracablity" of the treated water.

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Total Water Management Facility



Total Water Management Facility

B-1

B-2

B-3

Treatment process for flowback and produced waters

STATE IN MARK

7

Flowback and produced water pump from mountains

Treated flowback and produced waters storage

FracSTAR process that all waters must flow through for blending and treatment

Two Stage Filter:

Stage 1: 25 Micron

Stage 2: 10 Micron

FracSTAR process blends treated flowback and produced into fresh water while treating the fresh Water for bacteria and scaling index's

A-1

A-2

A-3

F-1

Moning tank

F-3

Working Tank F-4

This water was extremely turbid:

- SRB's at 10⁷ CFU
- APB's at 10⁵ CFU
- Iron Sulfide at 350 ppm
- H2S at 4 ppm
- pH at 5.8



STARTED OUT AS FRESH WATER

This water was not turbid and did not have H2S, Iron Sulfide and the pH was 7.2 going down hole

During the first 18 days of operation, 4,032 serial dilution bug bottles were used and 259 individual samples were taken from 18 different locations from within this operation to help adjust and develop the needed algorithmic equations and operational guidelines to achieve these goals in less than 30 days.

This water had some turbidity:

- SRB's at 10^o CFU
- APB's at 10° CFU
- Iron Sulfide at 0 ppm
- H2S at 0 ppm
- pH at 6.5



Treated REUSE and RECYCLE Water

This water is not turbid and does not have H2S, Iron Sulfide and the pH was 7.5 going down hole with no SRB's and or APB's "FRACABLE WATER"

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Treated REUSE and

RECYCLE Water

This water is not turbid and does not have H2S, Iron Sulfide and the pH was 7.5 going down hole with no SRB's and or APB's "FRACABLE WATER"



This water had some turbidity:

- SRB's at 10^o CFU
- APB's at 10° CFU
- Iron Sulfide at 0 ppm
- H2S at 0 ppm
- pH at 6.8

14 months of operation

48 wells

99.10% water reused & recycled

6,873,408 barrels / **288,683,136** gallons of fresh water conserved with an average disposal rate of **\$4.20** for disposal the producer saved **\$28,490,313.60** in disposal cost.



This process was piloted to run for a two well pad with 78 stages with a total of 507,000 Barrels / 21,294,000 Gallons of water to be consumed to Frac these two wells in 18 days. Here are the results of the process that ended up operating for 23 days due to the pump company having maintenance issues with their equipment.

Besides being very mobile it had to accomplish many goals to help make the Reuse and Recycle Project a successful and repeatable process certain KPI (Key Performance Indicators) had to be achieved.

- Oil Removal to <10 ppm
- Solids Removed with Turbidity < 20 NTU's
- Solids Dewatered > 95% Total Influent Volume of Recovered
- Total Iron < 5 ppm
- pH >6.5 and <7.8
- No living SRB's (Sulfate Reducing Bacteria)
- No Living APB's (Acid Producing Bacteria)
- 30,000 BPD (Barrels Per Day) within 18 hrs
- No Spills !!!!!

Process Through Put 30,000 Barrels Per Day in 18 Hours



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HINI





Oxidation and pH Adjustments ClO₂, NaCO₃, NaOH, Ba₂Cl, Polymer





Solids Concentration with Polymers

Munson #1002H

1007H

Muson 1003#

79

Solids Removal is discharged into bins

Dewatering of Solids for Disposal to Landfill



NCH CORPORATION Filtration & Polishing to reduce Post Precipitation





Filtration & Polishing Keep Solids Out of the Working Frac Tanks



INFLUENT WATER FLOWBACK & PRODUCED H2O

Total Days on RSW Pad 23.00

Total Barrels Treated 269,403.00

Total Gallons Treated 11,314,926.00

Total Pounds of Water Treated 102,859,466.30

Average Weight of Influent LBs/Gal 9.091

Average Weight of Enfluent LBs/Gal 9.086

Percent Total Water Weight Reduction 0.138%

SLUDGE GENERATION

Total Barrels of Sludge Generated 30,774.86

Total Gallons of Sludge Generated 1,292,544.00

Total Pounds of Sludge Generated 11,779,082.73

Average Weight of Sludge LBs /Gal 9.11



SOLIDS GENERATED FROM DECANTING SLUDGE

Total Barrels of Concentrated Sludge Generated 171.43

Total Gallons of Concentrated Sludge Generated 7,200.00

Total Weight of Concentrated Sludge in LBs 127,292.94

Average Weight of Haul Off LBs Per Gallon 17.68





WATER RECOVERD FROM SLUDGE

Total Barrels of Water Decanted from Sludge Generated 30,603.43

Total Gallons of Water Decanted from Sludge Generated 1,285,344.00

Average Weight of Recovered Water LBs/Gal

9.05

Percent Recovery of Water 99.443%

This Reuse and Recycle process when completed was successful in:

- Recovering over >99% of the water
- 1,100 Barrels of Oil
- 30,000 Barrels / 1,260,000 Gallons of Sludge that was Decanted to <200 Barrels 8,400 Gallons of Solids
- 0 SRB Bactria
- 0 APB Bacteria
- pH >6.8 and <7.5
- Two Stages completed with 100% Reuse & Recycled water (Fresh Water Pumps Failed)
- Average > 50% Reuse and Recycled Fracable Water

The water leaving the Reuse and Recycled Process was blended using FracStar on location with the untreated Fresh Water being treated for bacteria and a scale inhibitor being added on the fly the layout of the process is shown below. After the successes of the first mobile Reuse and Recycle treatment process the piloting of three more operations was approved and the summary of those processes was:

- >850,000 Barrels of Reuse and Recycled Water Treated
- >35,700,000 Gallons of Fresh Water Conserved
- >1,800 Barrels of Oil Recovered
- > 85,000 Barrels of Sludge Generated that was dewatered to < 450 Barrels of Disposal
- > 99% water recovery
- Calcium and Sulfate Scaling Indexes were lowered by >80%
- CO2 (Carbon Dioxide) Dissolved Gasses removed by >70%
- No H2S (Hydrogen Sulfide)
- No SRB's (Sulfate Reducing Bacteria) going down hole
- No APB's (Acid Producing Bacteria) going down hole
- pH > 6.85 and < 7.45



Another development occurred throughout this process that led to another evolution in the development of Reuse and Recycle applications.

This development however is tied to another upfront process which is significant in the ability to consume large volumes of water for Reuse and Recycle that helps reduce the need for additional fresh waters. In the application of the 4 Reuse and Recycle processes the FracStar application was being used for over a year to treat the fresh water being used in the Fracing Process. This had such a significant impact on the waters that were flowing back and being produced by the wells that the need for such a large mobile treatment process system was no longer needed and the foot print and speed of treatment evolved to a new level.

The on the fly Reuse and Recycle treatment process allows for the entire treatment process to occur on the frac pad and move with the pumping company. This also eliminates the risk of having a spill off location and on the ground due to a leaking or ruptured pipe.











Erergen Guadalupe 90% Frash 10% Arine

1.0m1C102

CIO_= 11.1ppm pH= 8.21





Energen Guadalupe 90% Fresh 10% Brine Untreated 0H= 8.44



This Reuse and Recycle process is constantly running:

- Recovering over >100% of the water
- 700 Barrels of Oil
- Averages 7,785 Barrels / 326,970 Gallons of Recycled Water
 Every Day
- 0 SRB Bactria
- 0 APB Bacteria
- pH >6.8 and <7.5



The this process has conserved 272,475 Barrels / 11,443,950 Gallons of Water to date.

The projected volumes conserved by end of 2014 1,498,612 Barrels / 62,941,725 Gallons of Water On another Reuse and Recycle process that was using 100% water flood water that had 1% to 2% Oil and >600 ppm H2S (Hydrogen Sulfide) and the presence of SRB and APB Bacteria which was to be 100% of the source water for a 13 Well Program. This water had to be treated to become Fracable and meet certain KPI (Key Performance Indicators) to insure the completion of the wells within the program which were:

- Turbidly <12 NTU's
- <0 ppm H2S (Hydrogen Sulfide)
- No SRB Bactria
- No APB Bactria
- >15 ppm of ClO2 (Chlorine Dioxide)
- pH >6.5 and <7.5
- 100% Reuse Water (No Fresh Water)
- No Water to be disposed of 100% Reuse & Recycle

This process had some safety challenges and previous processes failed to deliver the volume of water to do a 100% Reuse and Recycle and the water quality was affecting the Frac Performance with pressure and flow rate issues. These wells were projected to deliver 65 to 85 BPD (Barrels Per Day) based on the previous results from the Reuse and Recycled program used last year. This very small foot print supplied the water for all 13 wells and allowed for the treatment process to take place on a single shift each day of operating.



This process was so successful in the treatment of waters used for Reuse and Recycle that a number of developments occurred that had never been seen before:

- The treated Reuse and Recycle Water had pump times of 45 to 55 minutes, which allowed for this fluid to be used on Horizontal Fracs and not just Vertical Frac's
- Due to the length of the pump times and compatibility of the water with chemistry that was carrying the sand (proppant) down hole less Horsepower was needed to complete the wells (Major Cost Savings)
- The wells produced 75% to 100% more Oil than was projected (Major Money Maker) an increase from 75 BPD to 180 BPD

Due to these successes the implementation and use of the FracStar Process the expansion and development of this technology will help lead to the growth in Reuse and Recycle programs that will reduce the practice of disposing of water while consuming fresh water. With the enhanced well performance and major cost reductions in the implementation of Reuse and Recycle treatment programs the reduction and dependence on Fresh Water from the environment can start taking place.

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FracSTAR Summary

To date over 170,000,000 Barrels / 7,140,000,000 Gallons of water treated.

Over 1,000 analysis consisting of complete water and bacteria analysis pre, during, and post frac.

7,200,000 Barrels / 302,400,000 Gallons of water treated last month

15,200,000 Barrels / 638,400,000 Gallons of water treated last quarter.

389,050 Barrels / 16,340,100 Gallons of water averaged everyday.

100,000,000 Barrels / 4,200,000,000 Gallons of water projected for this year

Making Water "Fracable"

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